

Thermal generation of singlet oxygen ($^1\Delta_g\text{O}_2$) on ZSM-5 zeolite

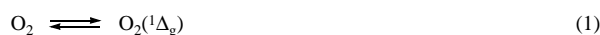
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Thermal generation of equilibrium $^1\Delta_g\text{O}_2$ in air at moderate temperatures and non-equilibrium thermal desorption of singlet oxygen from Ca–Cs/ZSM-5 zeolite were experimentally detected.

The participation of singlet oxygen ($^1\Delta_g\text{O}_2$) in the oxidation of hydrocarbons on heterogeneous catalysts was discussed previously.^{1–3} Data on the thermal desorption of $^1\Delta_g\text{O}_2$ from the Li–Sn–P–O system² and V_2O_5 catalysts³ were reported, and indirect evidence of the occurrence of $^1\Delta_g\text{O}_2$ at the surface of transition metal oxides was also obtained by EPR spectroscopy.¹ However, these results are inadequately reproducible, and until the present time there is no direct evidence of the participation of thermally generated $^1\Delta_g\text{O}_2$ in oxidation reactions (either homogeneous or heterogeneous), although the possibility of the direct thermal excitation of oxygen to a singlet state was considered by Turro.⁴ Moreover, the thermal generation of $^1\Delta_g\text{O}_2$ in an equilibrium concentration at moderate temperatures according to the reaction



(the reverse of the quenching of singlet oxygen) was not observed (probably, because of the absence of sensitive methods for the detection of $^1\Delta_g\text{O}_2$).

Previously,⁵ a sensitive chemiluminescence (CL) technique for the determination of extremely low concentrations of singlet oxygen in a gas phase was developed. This technique allowed us to perform continuous measurements of equilibrium $^1\Delta_g\text{O}_2$ concentrations in air at relatively low temperatures and to examine non-equilibrium thermal desorption of $^1\Delta_g\text{O}_2$ from zeolites.

The generation of singlet oxygen took place in an air flow (pressure of 60 Torr and linear velocity of 1.2 m s^{-1}) passed through a heated zone of a quartz tubular reactor (30 mm in length and 5 mm internal diameter). At the reactor outlet, the gas was rapidly cooled to ambient temperature and then arrived at a CL detector (for experimental detail, see ref. 5). Because the time of singlet oxygen quenching in air is rather long ($\sim 1 \text{ s}$ at 60 Torr and room temperature), the equilibrium $^1\Delta_g\text{O}_2$ concentration corresponding to the temperature of the heated zone of the reactor can be measured. In this case, the quenching of $^1\Delta_g\text{O}_2$ during the time it takes for air to be cooled and transferred to the CL detector is negligible.

The equilibrium $^1\Delta_g\text{O}_2$ concentration is determined by the expression [in the case of $C(^1\Delta_g\text{O}_2) \ll C(\text{O}_2)$]⁶

$$C(^1\Delta_g\text{O}_2) = C(\text{O}_2)(g_1/g_2)\exp(-E/RT) \quad (2)$$

where $C(^1\Delta_g\text{O}_2)$ is the equilibrium $^1\Delta_g\text{O}_2$ concentration in the gas phase at the temperature T ; $C(\text{O}_2)$ is the ground-state oxygen concentration (total oxygen concentration); g_1/g_2 is the electronic statistical weight ratio for the singlet and ground triplet states of oxygen, $g_1/g_2 = 2/3$ (ref. 6); E is the excitation energy of the oxygen singlet state (the enthalpy of formation of $^1\Delta_g\text{O}_2$).

Indeed, the intensity of the thermal formation of equilibrium $^1\Delta_g\text{O}_2$ was essentially the same on various catalysts (Ca–Cs/ZSM-5, the Li–Sn–P–O system and V_2O_5) and in an empty reactor. Figure 1 demonstrates a typical curve for this process. The energy E calculated from these data using equation (2) is 88.6 kJ mol^{-1} ($\pm 10\%$), which is consistent with $E = 94.2 \text{ kJ mol}^{-1}$, as found from spectroscopy data.¹ The corresponding preexponential factor $C(\text{O}_2)(g_1/g_2)$ is $\sim 6 \times 10^{17} \text{ molecule cm}^{-3}$ (the calculated value for air at 60 Torr and room temperature is $3.7 \times 10^{17} \text{ molecule cm}^{-3}$, the difference may be due to incorrect independent calibration of the CL detector at low $^1\Delta_g\text{O}_2$ concentrations).

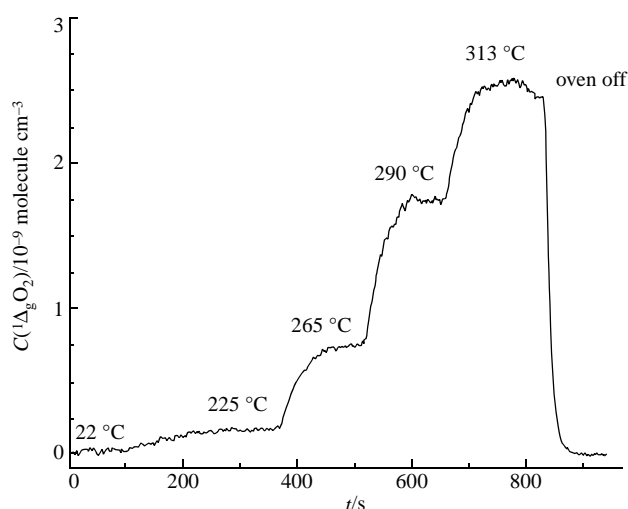


Figure 1 Thermal generation of equilibrium $^1\Delta_g\text{O}_2$ in an empty quartz reactor under conditions of a stepwise increase in the temperature (the detector was calibrated using a photochemical generator of $^1\Delta_g\text{O}_2$).

If a sufficient ballast volume or a glass filter was placed between the reactor and the CL detector, the signal vanished due to $^1\Delta_g\text{O}_2$ quenching. The same behaviour was observed in experiments when singlet oxygen was photochemically generated in a glass tube coated with methylene blue (in place of a heated reactor).

Taking into account all of the results, we can state with assurance that direct thermal generation of $^1\Delta_g\text{O}_2$ in equilibrium concentrations took place in our experiments. Note that a simple blank reactor can be used as a reliable standard source for calibration because the temperature dependence of $^1\Delta_g\text{O}_2$ concentration at the reactor outlet is determined by equation (2).

The Li–Sn–P–O and V_2O_5 catalysts generated $^1\Delta_g\text{O}_2$ only in equilibrium concentrations in our experiments. Thus, they exhibited no difference from an empty reactor.

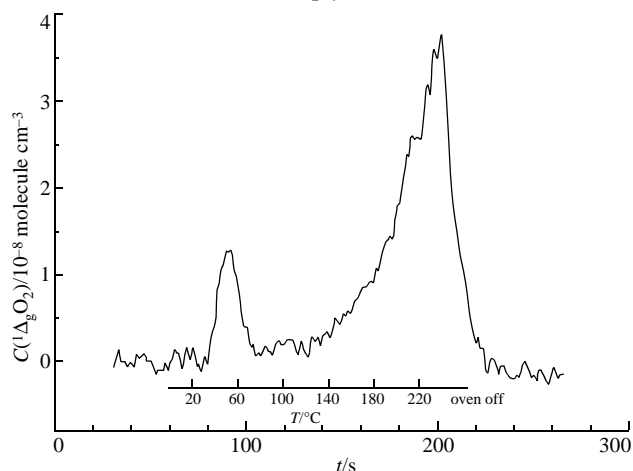


Figure 2 Non-equilibrium thermal desorption of $^1\Delta_g\text{O}_2$ from Ca–Cs/ZSM-5 zeolite under conditions of a linear increase in the temperature (the detector was calibrated with thermally generated equilibrium $^1\Delta_g\text{O}_2$ at the outlet of an empty quartz reactor).

The non-equilibrium generation of $^1\Delta_g\text{O}_2$ (i.e., in higher than equilibrium concentrations) was observed only on zeolite samples (ZSM-5 exchanged with alkaline and alkaline-earth cations). Figure 2 demonstrates a typical plot of the thermal desorption of $^1\Delta_g\text{O}_2$ from Ca-Cs/ZSM-5 zeolite. The sample was prepared from H-ZSM-5 (Si/Al ratio of 80) by continuous ion exchange in a 0.1 M CsNO_3 solution and then in a 0.1 M $\text{Ca}(\text{NO}_3)_2$ solution. Next, it was calcined at 650 °C in air for 4 h and exposed to dry air at room temperature for 16 h prior to the use in experiments.

It can be seen in Figure 2 that, in addition to the thermal generation of equilibrium $^1\Delta_g\text{O}_2$, which is detectable at temperatures higher than 140 °C, the curve exhibits a low-temperature peak of non-equilibrium thermal desorption of $^1\Delta_g\text{O}_2$ ($T_{\text{max}} = 55$ °C). This peak completely disappeared in the subsequent thermal desorption experiments. The capacity of the zeolite for non-equilibrium desorption of $^1\Delta_g\text{O}_2$ was restored after exposure to air at ambient pressure for 24 h.

It is obvious that, in this case, oxygen molecules adsorbed on the zeolite are the source of $^1\Delta_g\text{O}_2$. The reasons why the concentration of electronically excited $^1\Delta_g\text{O}_2$ in desorbed oxygen exceeds an equilibrium value are unclear. It is our opinion that the following factors can be responsible for this phenomenon: (i) stabilization of the $^1\Delta_g$ state of an adsorbed O_2 molecule as a result of splitting two degenerate π_g^* -orbitals¹ in strong electrostatic fields within zeolite channels ($\approx 10^{10}$ V m⁻¹ in ZSM-5)⁷ and (ii) differences in the activation energies of adsorption (and desorption) for the ground $^3\Sigma_g$ and excited $^1\Delta_g$ states of oxygen molecules, e.g., at the surface of MgO, $E_{\text{a ads}}(^1\Delta_g\text{O}_2) = 0$, while $E_{\text{a ads}}(^3\Sigma_g\text{O}_2) > 0$ (ref. 8).

Anyway, this experimental fact is the first example of the non-equilibrium thermal production of $^1\Delta_g\text{O}_2$ over heterogeneous catalysts (with the exception of the results,^{2,3} which were found to be irreproducible).

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